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# **The effect of different exchangeable cations on the CO<sup>2</sup> adsorption capacity of Laponite RD®**

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## **Abstract**

Tri-octahedral clay minerals have a potential to be used as  $CO<sub>2</sub>$  sorbents for intermediate temperatures (200-400 °C) owing to their thermal stability in this temperature range. In this study, laponite RD<sup>®</sup>, a commercially synthesized hectorite (with Na<sup>+</sup> as exchangeable cation) was used to investigate its capacity of  $CO<sub>2</sub>$  adsorption at 200 °C and ambient pressure. Different cations such as  $Co^{2+}$ , Ni<sup>2+</sup>, Mg<sup>2+</sup> and  $Ca^{2+}$  were employed to exchange Na<sup>+</sup> with the aim to study their effect on the capacity of adsorbing  $CO<sub>2</sub>$ . The commercial sample showed an adsorption capacity of 144  $\mu$ mol<sub>CO2</sub>/g. Most of other exchanged sample displayed a deficit in the quantity of  $CO_2$  adsorbed. An exception was the  $Ca^{2+}$ saturated sample, which exhibited a better performance (163  $\mu$ mol<sub>CO2</sub>/g) compared to the Laponite RD<sup>®</sup>. Thus, with higher affinity towards  $CO<sub>2</sub>$ , such sample could be a good candidate for  $CO<sub>2</sub>$  capture. For all samples, most of the CO<sub>2</sub> was desorbed, and the formation of carbonate bonds was not observed by FTIR spectroscopy suggesting that the  $CO<sub>2</sub>$  was mainly physisorbed.

**Keywords:** CO<sub>2</sub> adsorption, Laponite, cation exchange

#### **Introduction**

The release of  $CO<sub>2</sub>$  and other greenhouse gases due to human activities have contributed to the increase of atmosphere's temperature and subsequent climate change (Chevallier *et al.*, 2023). To limit the  $CO<sub>2</sub>$  release in the atmosphere different strategies are being studied. Great efforts are devoted to develop CO<sub>2</sub> capture and storage (CCS) technologies (Bui *et al.*, 2018). In addition to  $CCS$ ,  $CO<sub>2</sub>$  capture and utilization  $(CCU)$  is also being considered. The possibility to use CO<sup>2</sup> released from one industrial process to generate new chemicals in other process agrees well with circular economy principle. Thus, CCU technology development is also an attractive strategy in the effort to limit the  $CO<sub>2</sub>$  emissions. For example,  $CO<sub>2</sub>$  can be used to produce methane in a heterogeneous catalytic process called methanation or Sabatier reaction. Methane can be then used further as a fuel or as a feedstock for the production of chemicals. Sabatier reaction requires moderate temperature and pressure conditions (<400 °C, 1 bar), and CO<sup>2</sup> conversion is achieved in a presence of catalyst (Vogt *et al.*, 2019). Recently, integrated CCU (ICCU) technology has been proposed, where  $CO<sub>2</sub>$  is captured and then converted in a single fixed-bed reactor under isothermal conditions (Omodolor *et al.*, 2020). Such system is more economically viable than the two separate units, because it reduces the energy required for sorbent regeneration,  $CO<sub>2</sub>$  storage and transport. In such system, a dual functional material (DFM) can be used. DFM exhibit at the same time a considerable  $CO<sub>2</sub>$ capture capacity and favorable catalytic properties for  $CO<sub>2</sub>$  conversion. It means combining together a catalyst, which is sufficiently efficient for  $CO<sub>2</sub>$  conversion, and a supporting material, which exhibits relatively high  $CO<sub>2</sub>$  capture capacity.

In literature, layered double hydroxides (LDH) derived mixed oxides and MgO are reported as  $CO<sub>2</sub>$  sorbents for intermediate temperatures (200-400 °C) such as that corresponding to Sabatier reaction (Wang *et al.*, 2014). Although clay minerals have been investigated as sorbents of  $CO_2$  at low temperatures (<200 °C), their  $CO_2$  adsorption capacity has not yet been assessed at intermediate temperatures. Indeed, most of the  $CO<sub>2</sub>$  sorbents, which are efficient at low temperatures, loose their stability upon heating, *e.g.* amines and metal organic frameworks. Tri-octahedral (Mg-rich) clay minerals remain stable in the intermediate temperature range, and thus their  $CO<sub>2</sub>$  adsorption capacity should be evaluated and compared to that of LDH. The abundance and low cost of clay minerals make them an attractive  $CO<sub>2</sub>$ sorbent for industry even if their  $CO<sub>2</sub>$  adsorption capacity might be lower than other sorbents. This study investigated CO<sub>2</sub> adsorption on Laponite, tri-octahedral commercial clay with high surface (Christidis *et al.*, 2018) at 200 °C. The  $CO<sub>2</sub>$  adsorption is expected to decrease with the increase of temperature, thus the lowest limit, i.e.  $200\,^{\circ}\text{C}$  was chosen to assess the potential of Laponite for being used in such process. The sample was modified by a simple cation exchange to assess the effect of different exchangeable cations on  $CO<sub>2</sub>$  sorption capacity.

#### **Materials and Methods**

*Preparation of cation-exchanged samples.* Different chloride solutions were prepared to saturate commercial hectorite Laponite  $RD^{\circledast}$  with different cations such as  $Mg^{2+}$ ,  $Ca^{2+}$ ,  $Co^{2+}$ and  $Ni^{2+}$ . Laponite RD<sup>®</sup> (BYK-Chemie GmbH, Germany), magnesium chloride hexahydrate, MgCl<sub>2</sub>.6H<sub>2</sub>O (Sigma-Aldrich,  $\geq$  99.0 wt%), calcium chloride dihydrate, CaCl<sub>2</sub>.2H<sub>2</sub>O (Sigma-Aldrich,  $\geq$  99.0 wt%), nickel chloride hexahydrate, NiCl<sub>2</sub>.6H<sub>2</sub>O (Thermo Scientific, 99.3 wt%), cobalt chloride hexahydrate,  $CoCl<sub>2</sub>.6H<sub>2</sub>O$  (Acros Organics, 98.0 wt%) and deionized water of 18 MΩ.cm (Aquadem, PF 210, Veolia Water Technologies) were used. The cation-exchange process consisted of saturating the material with a highly concentrated chloride solution. 2.00 g (Precision Series, Fisherbrand) of Laponite RD were impregnated with 30 mL of 1 M chloride solution containing the exchangeable cation in a centrifuge tube. The tube was then agitated for at least 7 h before centrifugation at 8000 rpm (9946×*g*) for 10 min to remove the liquid phase (Rotanta 460, Hettich Zentrifugen). This step was repeated two times. Then the solid phase was washed with deionized water to remove the excess of chloride anions which was verified by adding  $Ag^+$  in the supernatant (AgNO<sub>3</sub>, Fluka, 99.0 wt%). The final product was oven-dried at 60 °C for 2 days (oven ED 056, Binder).

*Physicochemical characterization methods.* The structural properties of the samples were investigated by X-ray Diffraction (XRD) using a PANalytical MPD X'Pert Pro diffractometer (Almelo, The Netherlands) equipped with a Pixcel real-time multiple strip detector and operating with an angular aperture of 3.347° 2θ in the 2 to 70° 2θ range, and using CuKα radiation with a 0.15418 nm wavelength. XRD patterns were taken at 22 °C with a step size of 0.013° 2θ and a time per step of 218 s with the total time for acquisition of 1 h 15 mins. The divergence slit, the anti-scatter slit, and the two Soller slits were 0.0625, 0.125, and 2.3°, respectively.

Chemical composition of samples was determined using a wavelength dispersion X-ray Fluorescence (XRF) spectrometer Zetium from PANalytical (Almelo, The Netherlands). XRF experiments were carried out on pellets constituted of 0.3 g of the sample, pressed at 4 tons for 2 minutes.

Thermogravimetric analysis (TGA) of the samples was performed using a Mettler-Toledo TGA/DSC1 LF1100 apparatus (Switzerland), in alumina sample holders, under air, with a flow rate of 100 ml/min from 30 to 1000  $\degree$ C and a heating rate of 10  $\degree$ C/min. An empty sample holder was recorded as a reference to correct the baseline deviation.

Fourier transform infrared spectroscopy (FTIR) measurements were conducted using an Equinox IFS 55 apparatus (Karlsruhe, Germany) equipped with a DTGS detector from Bruker. The samples were mixed with KBr at a weight ratio of 1:100 and pressed at 4 bar for 2 min, followed by oven-heating at 200 °C. The spectrum obtained was the average of 200 scans with a resolution of  $4 \text{ cm}^{-1}$ . The spectrum was recorded with the software OPUS, which was also used to subtract  $CO<sub>2</sub>$  and  $H<sub>2</sub>O$  contributions.

N<sup>2</sup> adsorption-desorption isotherms were obtained on a Micrometrics ASAP 2420 equipment at -196 °C (Norcross, GA, USA). Prior to analysis, the samples were degassed at 300 °C for 15 hours and then again for 2 hours in the measurement emplacement. The degassing vacuum was 10<sup>-6</sup> bar. The Brunauer, Emmett, and Teller (BET) equation  $(0.01 < P/P_0 < 0.40)$  was used to calculate the specific surface area (SSA). The data were analyzed by means of the software MicroActive 5.02.

 $CO<sub>2</sub>$  *adsorption tests*. The  $CO<sub>2</sub>$  adsorption capacity of the samples was measured with a Setaram Sensys thermogravimetry-differential scanning calorimetry (TG-DSC) apparatus (France). The samples (around 15 mg) were first dehydrated at 300 °C under pure  $N_2$  flow (30 mL/min) then the temperature was decreased and stabilized to the adsorption temperature (200 °C) always under N<sub>2</sub> flow. Once the mass was stabilized, the gas was switched to  $CO<sub>2</sub>$ with a constant flow of 30 mL/min and maintained during the  $CO<sub>2</sub>$  sorption experiments (30 minutes) until complete saturation of the samples. Finally, the gas was switched back again to N<sup>2</sup> also for 30 minutes (**Figure 1**). The changes in mass were recorded in order to evaluate the  $CO<sub>2</sub>$  adsorption capacity of the materials. The pressure of gases during  $CO<sub>2</sub>$ adsorption experiments was 3 bar. The specification of gases used in the experiment were: CO<sub>2</sub> N45 (purity of 99.995% and impurities less than 50 ppm) provided by AirLiquid (France) and N<sub>2</sub> 4.5 (purity %  $\geq$  99,995) provided by Linde (France). Each experiment was performed twice, and the variation between the experiments did not exceed 5%.

**Figure 1.** Temperature profile for  $CO_2$  adsorption and desorption at 200 °C.

## **Results and discussion**

*Characterization of the exchanged materials.* All samples displayed a similar structure with characteristic diffraction peaks corresponding to tri-octahedral swelling clay minerals (**Figure 2**) (Brindley & Brown, 1982). The (00ℓ) reflections were almost absent suggesting disordered stacking and /or low crystallinity. The broad peaks corresponding to (hkl) planes confirmed that all samples had small coherent scattering domain size. The similarity in XRD traces between Laponite RD and the exchanged samples showed that the crystal structure of original material was not impacted by the exchange protocol. No other additional crystalline phase precipitation occurred.

**Figure 2.** Powder X-ray diffraction patterns of Laponite® saturated with different cations.

FTIR analysis confirmed that all peaks were similar between the samples indicating that the basic structure of Laponite was not altered during the exchange process (**Figure 3**). The absorption bands such as stretching of O–H at 3680 cm<sup>-1</sup>, of Si–O at around 1010 cm<sup>-1</sup>, the bending of O–H at 657 cm<sup>-l</sup> and Si–O at 450 cm<sup>-l</sup> could be observed, characteristic of hectorite (Ogawa *et al.*, 2008; Yuan *et al.*, 2008; Yang *et al.*, 2022). Despite of the drying the pellets at 200 °C before the analysis, the bands attributed to bound water at 3445 and 1637 cm<sup>-1</sup> were still present, however, their intensity was not significant compared to other characteristic bands of the samples.

**Figure 3.** FTIR spectra of Laponite® saturated with different cations.

The chemical composition of the samples determined by XRF (**Table 1**) confirmed that the exchangeable Na<sup>+</sup> present in Laponite RD was replaced by  $Ni^{2+}$ ,  $Co^{2+}$ ,  $Mg^{2+}$  and  $Ca^{2+}$ . No sodium was detected by XRF in the exchanged samples.

<b>Element</b>	Laponite $(\%at)$	Ni_Lap $(\%at)$	$Co_{Lap}$ $(\%at)$	Mg_Lap $(\%at)$	$Ca_{Lap}$ $(\%at)$
O	59.83	55.75	54.88	49.04	48.43
Mg	14.15	14.19	14.26	18.57	16.98
Si	23.94	25.49	25.90	32.25	31.63
Ca					2.85
Ni		4.32			
Co			4.83		
Na	1.80				

Table 1. Chemical composition of Laponite® saturated with different cations determined by XRF.  $\overline{\mathbb{R}}$ 

The  $N_2$  physisorption isotherms of the Laponite samples were collected to determine their specific surface area (**Figure 4**). According to the IUPAC classification (Thommes *et al.*, 2015), all sample isotherms were of type IVa and hysteresis loop of type H3, indicating the presence of a mesoporous network with lamellar particles and fissure structures (Chen *et al.*, 2013). The samples showed relatively high surface areas ranging from 377 to  $408 \text{ m}^2/\text{g}$ (**Table 2**) compared to other common clay minerals. For Na-montmorillonite the specific surface area was reported to be  $23 \text{ m}^2/\text{g}$  (Dogan *et al.*, 2006). Such high surface area of Laponite compared to natural sample was due to the synthetic origin, which was influenced

by production process (smaller particle size, particular dispersion and drying techniques). An improved adsorption of  $CO<sub>2</sub>$  compared to other common clay minerals could then be expected due to the high contact area with  $CO<sub>2</sub>$  molecules. The cation exchange had insignificant effect on the surface area of the samples.

**Figure 4.** N<sub>2</sub> adsorption (filled symbols) / desorption (empty symbols) isotherms of Laponite® saturated with different cations.

**Table 2.** Specific surface area and the amount of  $CO_2$  adsorbed / desorbed of Laponite® saturated with different cations.

	Laponite	Ni_Lap	$Co$ _Lap	Mg_Lap	$Ca_{Lap}$
SSA $(m^2/g)$	377	386	405	408	389
$CO2$ ads (µmol/g)	144	68	60	93	163
$CO2$ des (µmol/g)	129	55	52	80	138

To evaluate the thermal stability of samples, TGA was performed and the profiles were recorded (**Figure 5**). All samples exhibited similar profiles with the first mass loss at around 100 °C of about 13-14 wt% related to the dehydration. The second mass loss at around 765 °C of about 4-5 wt% was related to the dehydroxylation of the materials to form the corresponding mixed oxides (Earnest, 1983a; b). In general, all samples had a thermal stability between 200 and 650 °C which is desirable for a potential application as  $CO_2$  sorbent in dual functional materials.

**Figure 5.** TG curve and its derivative of Laponite® saturated with different cations. For all samples, the TG profiles are shown on the left axes and the DTG profiles are shown on the right axes.

 $CO<sub>2</sub>$  *adsorption tests*. **Figure 6** illustrates the amount of  $CO<sub>2</sub>$  adsorbed and desorbed at 200 °C for Laponite and cation exchanged samples. The Laponite adsorbed  $144 \mu$ mol CO<sub>2</sub> per gram. As the cations were exchanged, a significant change appeared in  $CO<sub>2</sub>$  adsorption capacity of the samples. The samples Co\_Lap and Ni\_Lap showed an adsorption capacity reduced to less than half  $(60-68 \mu m o l/g)$  compared to the Laponite. Mg Lap performed better than the previous two samples but still less  $CO<sub>2</sub>$  was adsorbed compared to Laponite. The only sample that surpassed Laponite was the Ca\_Lap where 163  $\mu$ mol CO<sub>2</sub>/g were adsorbed (13% higher compared to the Laponite). These results showed that among the cations that were exchanged,  $Ca^{2+}$  proved to be the one that had the best affinity with  $CO<sub>2</sub>$  molecules.

**Figure 6.** Amount of CO<sub>2</sub> adsorbed/desorbed at 200 °C after a pre-treatment at 300 °C under

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As it can be seen in **Table 2**, the  $CO<sub>2</sub>$  adsorption capacity was not correlated to the specific surface area (SSA) of samples. Ca\_Lap sample had the highest amount of  $CO<sub>2</sub>$  adsorbed while it represented an average specific surface. Thus, the difference in  $CO<sub>2</sub>$  adsorption capacity of different materials was not due to the SSA but influenced by the affinity of different cations towards  $CO<sub>2</sub>$ . It has to be noted that the SSA determined with  $N<sub>2</sub>$  physisorption represented only the external surface of the material as the  $N_2$  molecules were not able to enter the

interlayer space. However, the  $CO<sub>2</sub>$  adsorbed molecules could be potentially adsorbed not only on the external surface, but also on the interlayer surface due to the fact that the  $CO<sub>2</sub>$ molecules are much smaller in size. Sample characterization by XRD and FTIR showed that the structure of material remained the same, thus the type of sites on the surface would also be expected to remain the same, the only difference being the exchangeable cations. Therefore, we hypothesize that the difference in  $CO<sub>2</sub>$  adsorption among the samples was related to the basicity of the respective cations. Indeed, as  $CO<sub>2</sub>$  is considered a Lewis acid, it tends to react with the most "basic" cation among those present after exchange. The pKa values provide insight into the basicity of cations in solution, where a higher pKa indicates greater basicity. With a pKa of 12.70, the  $Ca^{2+}$ <sub>aq</sub>/CaOH<sup>+</sup><sub>aq</sub> pair exhibits higher basicity compared to the corresponding pairs of Mg (pKa = 11.40), Ni (pKa = 9.86), and Co (pKa = 9.80). Consequently,  $Ca^{2+}$  demonstrates the strongest affinity for  $CO_2$  molecules due to its superior basicity. Laponite sample contained  $Na^+$  and  $Mg^{2+}$  as exchangeable cations. For this reason, the adsorption of  $CO<sub>2</sub>$  for Laponite sample was higher than that of Mg. Lap sample, which did not contain Na<sup>+</sup>, but only  $Mg^{2+}$ . The adsorbed amount of  $CO_2$  was smaller for Ni\_Lap and Co\_Lap samples compared to Mg\_Lap, Lap (Mg+Na) and Ca\_Lap samples due to the smaller basicity of Ni<sup>2+</sup> and  $Co^{2+}$  as compared to Mg<sup>2+</sup>,  $Ca^{2+}$  and Na<sup>+</sup>.

The  $CO<sub>2</sub>$  desorption was performed by switching the inlet gas back to  $N<sub>2</sub>$  during 30 minutes. As shown in **Figure 6**, all samples desorbed 80-90% of the amount  $CO_2$  adsorbed. These  $CO_2$ molecules could be then expected to be as physiosorbed. The remaining  $10\n-20\%$  of  $CO<sub>2</sub>$ molecules could either be trapped within the porous structure or bonded chemically with the cations to form the corresponding carbonates. A FTIR analysis was performed on the Ca\_Lap sample after it underwent the  $CO<sub>2</sub>$  adsorption-desorption test. A comparison between the same sample before and after  $CO<sub>2</sub>$  test is shown in **Figure 7**. It can be seen that main band corresponding to carbonate at  $1460 \text{ cm}^{-1}$  (Munawaroh *et al.*, 2019) was not observed.

Calcium carbonate has two additional bands which are less intense at 880 cm<sup>-1</sup>, and 712 cm<sup>-1</sup>. A small change was observed for Ca\_Lap sample after  $CO_2$  adsorption around 800 cm<sup>-1</sup>, but the absence of the most intense carbonate band suggested that there were no carbonates formed.

**Figure 7.** FTIR spectra of Ca\_Lap before (black line) and after the CO<sub>2</sub> adsorption test (red

line).

 $CO<sub>2</sub>$  gas phase band values are 2349 and 667 cm<sup>-1</sup> respectively, but no band was observed around 2349 cm<sup>-1</sup> in our study, and the band at  $667 \text{ cm}^{-1}$  overlapped with the strong band of O-H bending in material structure.

The materials studied in this paper were compared to other potential materials for  $CO<sub>2</sub>$ adsorption (**Table 3**). For intermediate temperatures (200-400 °C), two types of materials have been reported in the literature as  $CO<sub>2</sub>$  sorbents: mixed oxides derived from LDH and MgO.

<b>Material</b>	<b>Name</b>	<b>SSA</b>	CO <sub>2</sub>	<b>Reference</b>
		$(m^2/g)$	adsorbed	
			$(\mu mol/g)$	
Mg-Al 3:1 $CO_3^2$	$Mg_3Al_1$ -CO <sub>3</sub>	154	720	(Gao et
				al., 2013)
Mg-Al 3:1 $CO32$ nano	LDH (IEP)	103	580	(Wang et
				al., 2013)
Mg-Al 3:1 $CO_3^2$	$Mg_3Al_1$ -CO <sub>3</sub>	239	530	(Wang et
				al., 2011)
Mg-Al 3:1 $CO_3^2$	$Mg_3Al_1$	239	410	(Wang et
				al., 2010)
Mg-Fe 3:1 $CO_3^2$	$Mg_3Fe_1$	255	462	(Wang et
				al., 2010)
Li-Al 3:1 $CO_3^2$	$LiAl2-CO3$	199	510	(Huang et
				al., 2014)
Mg-Al 3:1 $CO32$ C16	LDH-C16	348	910	(Qin et al.,
				2017)
Mg-Al 3:1 $CO_3^2$ <sup>-</sup> nano +	$K2CO3 -$	n.d.	1210	(Wang et
$K_2CO_3$	LDH (IEP)			al., 2013)
MgO	MgO		841	(Han et
				al., 2012)
MgO-Al <sub>2</sub> O <sub>3</sub> aerogel	5A5M		2977	(Han et
				al., 2012)
MgO - biomass ash	MgO-RHA-		4560	(Guo $et$
	20			al., 2020)
<b>Laponite RD</b>	Lap	377	144	This work
$Ca^{2+}$ -saturated Lap	Ca_Lap	389	163	This work

**Table 3.** Comparison of the  $CO_2$  adsorption capacity at 200  $\degree$ C/ 1 atm between Laponite cation-exchanged materials in this work and other materials from literature.

LDH with molar ratio Mg:Al of 3:1 and  $CO_3^2$  as a charge compensating anion was reported to adsorb from 410 to 720  $\mu$ mol/g of CO<sub>2</sub> (Table 3). Other charge compensating anions such as nitrates or chlorides decreased  $CO<sub>2</sub>$  adsorption capacity (Wang *et al.*, 2011). Replacement of Mg by Li or Al by Fe as well as the incorporation of organic acids slightly increased  $CO<sub>2</sub>$ adsorption capacity. The most efficient LDH modification was with  $K_2CO_3$  where the material capacity to adsorb  $CO<sub>2</sub>$  was doubled from 600 to 1210  $\mu$ mol/g. Further combination of alkali doping and organic acid-modification increased the LDH-based material adsorption

to 1930  $\mu$ mol/g (Qin *et al.*, 2017). Other material reported for intermediate-temperature  $CO<sub>2</sub>$ capture was MgO. In a form of aerogel, it represented the  $CO<sub>2</sub>$  adsorption capacity much higher compared to that of LDH (2977 µmol/g). The modification with biomass ash increased materials  $CO_2$  adsorption capacity even more (4560  $\mu$ mol/g). Despite excellent  $CO_2$ adsorption values, MgO was reported to present a problem of sintering which would decrease CO<sub>2</sub> adsorption capacity in long term (Zhao *et al.*, 2024).

Pristine Laponite tested in this study had approximately four times smaller  $CO<sub>2</sub>$  adsorption capacity compared to LDH and MgO. The modifications, such as cation exchange tested here, slightly increased  $CO<sub>2</sub>$  adsorption capacity, but the results were still not competitive with LDH.

In order to compare Ca\_Lap with other clay minerals materials for which the  $CO<sub>2</sub>$  adsorption was performed at room temperature or lower, additional  $CO<sub>2</sub>$  adsorption experiments were performed. The pretreatment was done at 300  $^{\circ}$ C under N<sub>2</sub> flow as previously, but the adsorption of  $CO_2$  was performed at 100 and 30 °C instead of 200 °C. As expected, the amount of  $CO_2$  adsorbed increased. At 100 °C, Ca\_Lap adsorbed 360 µmol/g and at 30 °C the adsorbed  $CO_2$  value was 692  $\mu$ mol/g. This value is similar or slightly higher compared to the values reported in the literature. Stevens *et al.* (2013) reported a CO<sub>2</sub> adsorption capacity of 490 µmol/g at 25 °C for K10 montmorillonite sample, and Azzouz *et al.* (2009) reported 685 µmol/g for Na montmorillonite.

Thus, Laponite had  $CO_2$  adsorption capacity close to other smectites, but the amount of  $CO_2$ adsorbed per g of material was significantly lower compared to other materials reported in intermediate temperatures (200-400 °C), e.g., LDH and MgO.

## **Conclusion**

In this work, we investigated the effect of the different cations exchanged with  $Na<sup>+</sup>$  of a Laponite  $RD^{\circledast}$  on  $CO_2$  adsorption capacity. The samples were characterized throughout a series of physico-chemical methods which confirmed that the sample structure was not altered during the cation exchange process, and that the Na<sup>+</sup> was replaced by  $Co^{2+}$ , Ni<sup>2+</sup>, Mg<sup>2+</sup> and Ca<sup>2+</sup>, respectively. With a CO<sub>2</sub> adsorption capacity at 200 °C of 163 µmol/g, the Ca<sup>2+</sup>saturated laponite (Ca\_Lap) outperformed the other prepared samples and also was the only sample that outperformed the Laponite itself. This difference in  $CO<sub>2</sub>$  adsorption was related to the affinity of the cation with  $CO_2$  and as  $Ca^{2+}$  had the best affinity, Ca Lap adsorbed the most  $CO_2$  among the samples. Furthermore, evidence from the infrared analysis after the  $CO_2$ adsorption indicated that the  $CO<sub>2</sub>$  molecules were mostly physically adsorbed. High  $CO<sub>2</sub>$ adsorption capacity at 200  $\degree$ C is one of the criteria for selecting materials for CO<sub>2</sub> capture and utilization process. Laponite had  $CO<sub>2</sub>$  adsorption capacity close to other similar clay minerals, but the amount of  $CO_2$  adsorbed per g of material was significantly lower compared to other materials reported in intermediate temperatures (200-400 °C), e.g. LDH and MgO.

# **Credit author statement**

**Minh Hoang Nguyen:** Data curation; Resources; Methodology; Investigation; Formal analysis; Visualization; Writing - original draft; Writing - review & editing. **Liva Dzene:** Conceptualization; Funding acquisition; Project administration; Supervision; Resources; Methodology; Formal analysis; Validation; Writing - review & editing. **Simona Bennici:** Conceptualization; Resources; Funding acquisition; Project administration; Supervision; Validation; Writing - review & editing. All authors have read and agreed to the published version of the manuscript.

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Figure 4:



Figure 5:



Figure 6:



Figure 7:

