



RESEARCH ARTICLE

On the turbulent viscosity parameter C_μ in the k - ϵ model

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Abstract

The Reynolds-averaged Navier–Stokes (RANS) models depend on empirical constants to close the Reynolds stress terms. The empirical constants were obtained using experiments conducted at low Reynolds numbers several decades ago. In this paper, we revisit the turbulent viscosity parameter C_μ , based on the stress–intensity ratio $c^2 = |\overline{uw}|/k$. Here, $|\overline{uw}|$ and k are the absolute values of the Reynolds stress and turbulent kinetic energy, respectively. Through *a priori* comparisons, we find that the currently accepted value of $C_\mu = 0.09$ does not agree with the latest direct numerical simulation (DNS) and experimental datasets of wall-bounded turbulent planar flows. Therefore, a new value is suggested by averaging c^2 in the equilibrium region, where the production (\mathcal{P}) of k is within 10% of the dissipation rate (ϵ), and consequently, $c^4 \approx C_\mu$. We evaluate flows up to friction Reynolds number $Re_\tau \approx 10\,000$ and find that with increasing Re_τ , C_μ approaches a value of 0.06, which is almost 50% lower than the prevalent value of 0.09. Finally, we perform an *a priori* test with the new (proposed) value of $C_\mu = 0.06$ to show that the estimated turbulent viscosity ν_T for wall-bounded flows is in much closer agreement with the exact (DNS) values than when ν_T is estimated using $C_\mu = 0.09$.

Impact Statement

Reynolds-averaged Navier–Stokes (RANS) simulation of the fluid flow is integral to modern engineering design. It has enabled the application of computational fluid dynamics (CFD) to various engineering problems. The current configuration of RANS model over-predicts the turbulent viscosity, affecting the accuracy of the model. To overcome the limitation, RANS users must calibrate their models to achieve the desired results. Calibration is required to compensate for the inappropriate model constants used since the first estimate of the stress intensity ratio, five decades ago. Through this study, we motivate the need to update the value of C_μ to 0.06 to better align RANS models with the flow dynamics revealed through the latest direct numerical simulation (DNS) and show that the correction of turbulent viscosity parameter C_μ leads to better prediction of turbulent viscosity ν_T for wall-bounded flows. A similar correction is required for other canonical flows when suitable high-fidelity datasets are available. We hope that the insights from this paper will motivate the CFD community to revisit the other empirical constants used in RANS models to reflect the latest findings obtained from DNS and experiments that will keep the RANS modelling relevant.

1. Introduction

The k - ϵ model has been one of the most popular turbulence models used in engineering over the last several decades to close the Reynolds-averaged Navier–Stokes (RANS) equations. The RANS turbulence models' robustness and computational efficiency have led to their wide acceptance in commercial codes. Even though they are imperfect, RANS models provide preliminary insights that greatly reduce the cost of engineering design for practical applications. However, in the last few decades, there has been little advancement in RANS modelling. The limitations of the RANS models have not been adequately addressed and essential updates in light of improved experiments and direct numerical simulation (DNS) have eluded the research community's focus. Therefore, due to stagnation in RANS modelling, the focus has now shifted to more computationally expensive techniques such as DNS and large eddy simulation (LES) (Bush *et al.* 2019) to solve the emerging problems in fluid dynamics.

We believe that RANS, while not a panacea, provides valuable insights into flows of practical interest, as shown in recent works by Boikos *et al.* (2024), Sinclair, Venayagamoorthy & Gates (2022) and Rodi (2017). Twenty years ago, Hanjalic (2005) correctly predicted that despite the growth of LES, RANS will continue to be a popular design tool. Durbin (2018) highlighted that developments in RANS modelling have not kept up with their increasing use in the industry, and RANS will remain relevant for CFD applications. Therefore, instead of discarding them in favour of advanced techniques, critical revisits, as shown in this paper, will improve RANS modelling and keep it relevant for solving engineering problems.

1.1. RANS modelling and k - ϵ model

RANS modelling is required to close the Reynolds stress term $\overline{u_i u_j}$ obtained by ensemble averaging of the instantaneous Navier–Stokes equation. In a fully developed planar shear flow, as discussed in this paper, the non-diagonal terms of the Reynolds stress tensor $\overline{u_i u_j}$ reduce to \overline{uw} . Here, u_i is the velocity fluctuation, and for a planar case, u , v and w are fluctuations in the streamwise, spanwise and wall-normal directions, respectively. Among different techniques used to model the Reynolds stress term (refer to Pope (2000) and Durbin & Shih (2005) for an overview of closure methods), the k - ϵ model (Lauder & Spalding 1974) has emerged as one of the most ubiquitous and popular closure models.

Using the turbulent viscosity hypothesis (TVH) in a linear eddy-viscosity model, the Reynolds stress \overline{uw} is expressed in terms of turbulent viscosity ν_T and mean shear $S = dU/dz$, where U is the mean streamwise velocity, as

$$\overline{uw} = -\nu_T \frac{dU}{dz}. \quad (1.1)$$

For closure, S can be measured, but ν_T needs to be estimated. Dimensional reasoning implies that $\nu_T \sim [L^2/T] \sim [L/T \times L]$; therefore, ν_T can be expressed as a product of a length scale l^* and a velocity scale u^* . As suggested by Kolmogorov (1941) and Prandtl (1945), u^* can be assumed to scale as $ck^{1/2}$, where $k = \overline{u_i u_i}/2$ is the turbulent kinetic energy. In the near-wall region, $u^* = l^* S$. From the definition of ν_T , (see (1.1)), $u^* = (\overline{|uw|})^{1/2}$. Thus, $c = (\overline{|uw|}/k)^{1/2}$ and its square $c^2 = \overline{|uw|}/k$ is called the stress–intensity ratio. If a length scale l^* is defined, then the transport equation for k can be solved. Under the assumption of equilibrium (Richardson–Kolmogorov cascade), $\epsilon \sim u^{*3}/l^* \Rightarrow \epsilon \sim k^{3/2}/l^* \Rightarrow \epsilon = Ck^{3/2}/l^*$, where C is another model constant. Therefore,

$$\nu_T = cC \frac{k^2}{\epsilon}. \quad (1.2)$$

Alternatively, as suggested by Harlow & Nakayama (1968), $\epsilon \sim k^{3/2}/l^* \Rightarrow l^* \sim k^{3/2}/\epsilon$. Since $u^* \sim k^{1/2}$, $\nu_T \sim k^2/\epsilon$. By assuming that ν_T depends only on k and ϵ , a turbulent viscosity parameter, C_μ , is

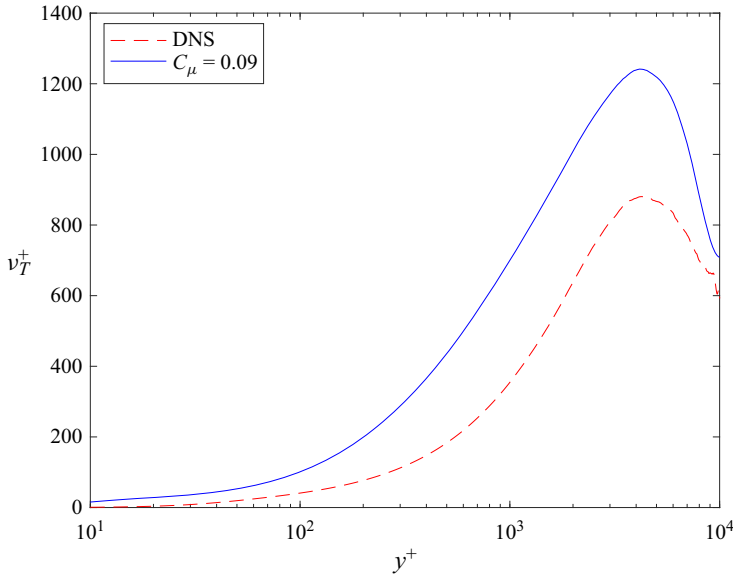


Figure 1. A priori test showing the turbulent viscosity ν_T using DNS data for $Re_\tau = 10000$ (Hoyas *et al.* 2022).

introduced to obtain

$$\nu_T = C_\mu \frac{k^2}{\epsilon}. \quad (1.3)$$

Equation (1.3) is the specification of ν_T in the k - ϵ model. The standard k - ϵ eddy-viscosity model uses $C_\mu = 0.09$, proposed by Jones & Launder (1972). From (1.1) and (1.3), $C_\mu = -\overline{uw}/(Sk^2/\epsilon)$. Evidently, this is not a constant. To obtain closure for \overline{uw} , an independent estimation of C_μ is required. After the initial proposal of a constant C_μ , a minor correction to the C_μ was implemented based on the turbulent Reynolds numbers $Re_T = k^2/\nu\epsilon$ for low-Reynolds-number flows such that at higher Re_T , C_μ approached 0.09 (Jones & Launder 1973). For free shear flows, a correction to C_μ based on Rodi's (1972) work was made by Launder *et al.* (1973) based on S . Additionally, in wall-bounded flows, to improve the near-wall behaviour, parametrization of C_μ in terms of S was proposed by Cotton *et al.* (1992) and later improved by Cotton & Ismael (1998), Suga (1995) and Karimpour & Venayagamoorthy (2014). Further, Reynolds (1987) and Shih *et al.* (1995) have argued that parametrization of C_μ is necessary as the model becomes unrealizable in the presence of a large S due to reduction in the value of C_μ . However, the parametrization of C_μ has not been popular because, away from the wall, S reduces dramatically and poses numerical challenges in the implementation. Further, all such parametrizations of C_μ have not been derived independently but are based on the local equilibrium value of 0.09. We will henceforth demonstrate the inaptness of the hitherto used value of $C_\mu = 0.09$ using an *a priori* test and suggest improvements.

1.2. A priori test of ν_T using DNS data

We perform an *a priori* test using the DNS of high-Reynolds-number channel flow ($Re_\tau = 10000$). In figure 1, it is evident that $C_\mu = 0.09$ causes an over-prediction of ν_T by almost 50%. Thus, the current value of C_μ must be revised to align the k - ϵ model with the latest experimental and DNS values.

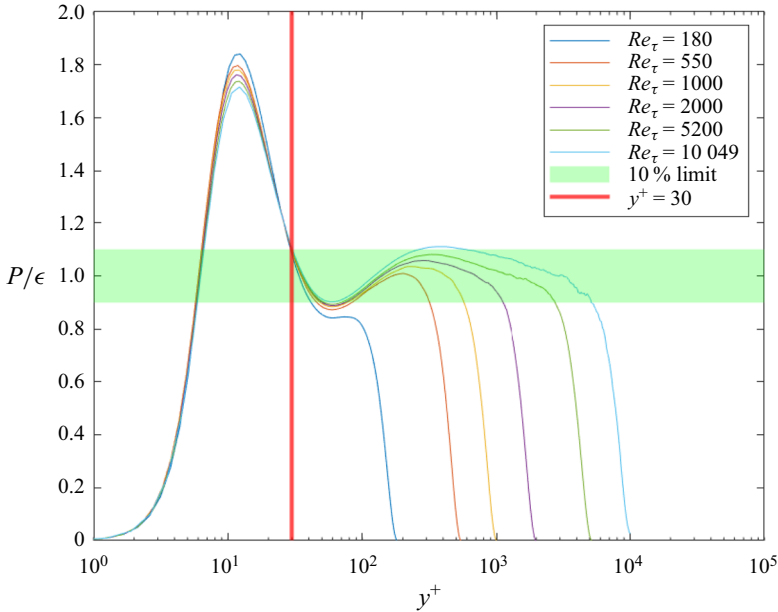


Figure 2. Ratio of production rate to dissipation rate of the turbulent kinetic energy P/ϵ for different Re_τ values from DNS of channel flow. The equilibrium region with 10 % tolerance is shown in the green patch.

1.3. Equilibrium region and relationship between c , C and C_μ

The transport equation of k for a fully developed flow contains rate of production term $\mathcal{P} = -\overline{uw}S$ and dissipation rate term ϵ . When $\mathcal{P} \approx \epsilon$, the flow is said to be in equilibrium. The dissipation follows the Richardson–Kolmogorov cascade (Vassilicos 2015). Figure 2 shows the ratio \mathcal{P}/ϵ for different Re_τ across the depth of the flow. For the majority of the flow depth, \mathcal{P} is within 10 % of ϵ . We know that in the logarithmic region, $u^* = l^*S \Rightarrow l^* = u^*/S$. By equating (1.3) and (1.1), and using $u^* = ck^{1/2}$, we get $C = c^3$. Therefore, by careful rearrangement and substitution, the relationship between constants c , C and C_μ , as shown in (1.4) and (1.5), are obtained:

$$c^2 = C_\mu^{1/2} \left(\frac{\mathcal{P}}{\epsilon} \right)^{1/2}, \tag{1.4}$$

with $\mathcal{P} \approx \epsilon$,

$$C_\mu \approx c^4. \tag{1.5}$$

The value of the turbulent viscosity parameter C_μ has been determined using empirical estimates of the stress intensity ratio c^2 . The hitherto value of C_μ emanates from the experimental findings of Champagne, Harris & Corrsin (1970), who reported asymptotic values of $|\overline{uw}|$, u , v and w using wind-tunnel experiments from which c^2 could be calculated as 0.32 for $Re_\tau \approx 3000$. Jones & Launder (1973) and Launder & Spalding (1974) used 0.33 to close their model. The experiments by Tavoularis & Corrsin (1981) and Harris, Graham & Corrsin (1977) confirmed the findings of Champagne *et al.* (1970) at low Reynolds numbers. Even before Jones & Launder (1972), Bradshaw, Ferriss & Atwell (1967) used an approximate value of 0.3 to substitute for c^2 , but they cautioned against indiscriminate use of this constant. Later, Yakhot & Orszag (1986) theoretically derived a value of $C_\mu = 0.085$ for a variant of the k – ϵ model for high-Reynolds-number flows. As will be shown later, turbulent viscosity ν_t predicted using $C_\mu = 0.085$ does not agree with the high-Reynolds-number DNS results. Thus, Champagne *et al.*'s

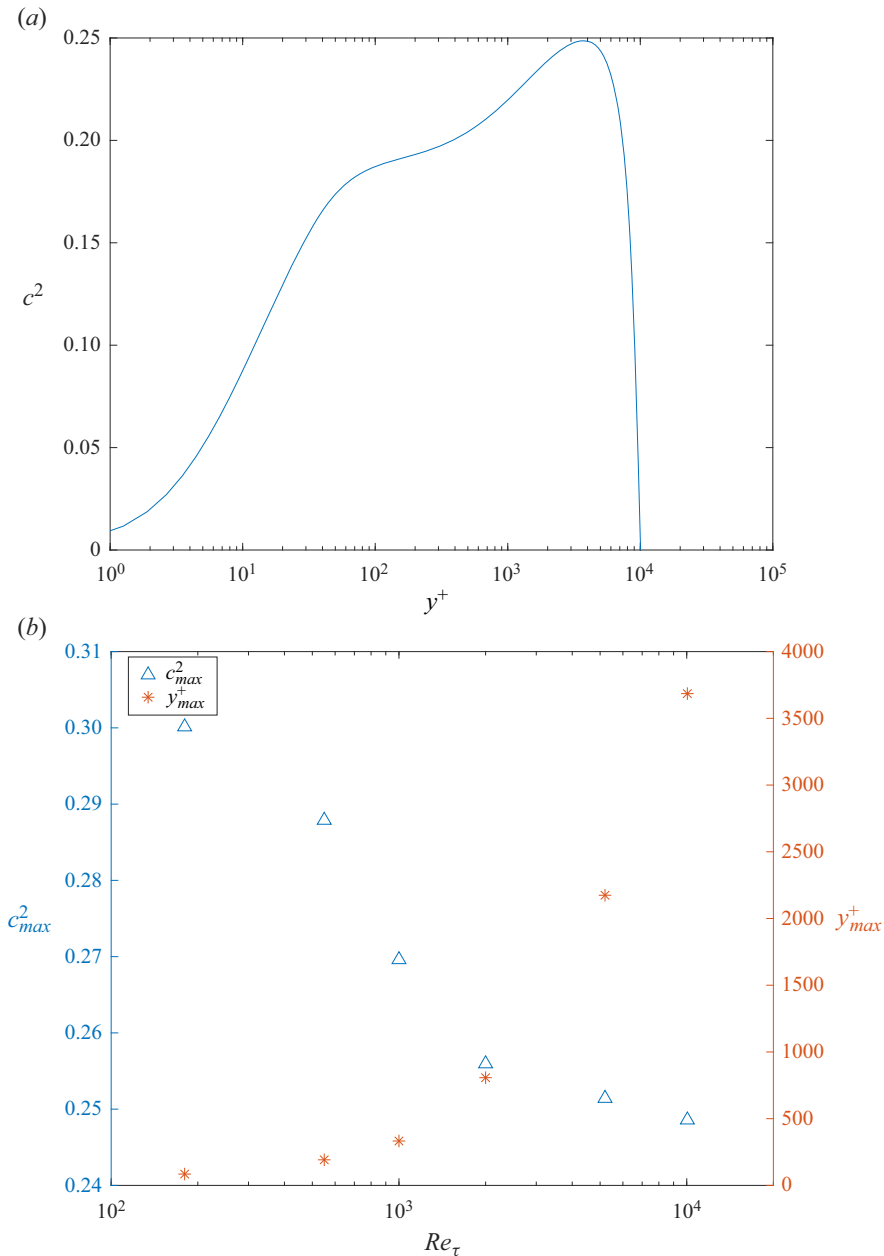


Figure 3. (a) Variation of $c^2 = |\overline{uw}|/k$ is plotted at $Re_\tau = 10000$ from DNS data (Hoyas et al. 2022); (b) maximum values of c^2 are plotted with increase in the Re_τ as given by the left-vertical axis and their corresponding locations are also plotted as given by the right-vertical axis.

(1970) experimental observations are unsuitable for high-Reynolds-numbers flows. The latest findings using the DNS datasets suggest much lower values of c^2 , as shown in figures 3(a) and 3(b).

In figure 3(a), it can be observed that c^2 is not a constant and the peak is just under 0.25. Moreover, as inferred from figure 3(b), the peak values of c^2 decrease with increasing Re_τ and, even for the lowest $Re_\tau = 180$, the peak is lower than 0.3. Therefore, C_μ must be less than 0.09 (see (1.5)).

Recently, Xu, Sun & Xu (2020) analysed the behaviour of c^2 for different canonical flows but did not discuss its implication on C_μ .

Despite their limitations, linear eddy–viscosity models, such as the k – ϵ model, have been extremely popular because of the ease of implementation and their computational efficiency. Therefore, a constant C_μ simplifies the model and adds to its acceptance in widely used commercial codes. However, since c^2 is not a constant, using an obsolete constant for C_μ can lead to high uncertainties in the RANS model. Duraisamy, Iaccarino & Xiao (2019) have emphasized that model constants (C_μ , C_{ϵ_1} etc.) are the major source of uncertainty in RANS modelling. Several works have attempted to quantify the uncertainty in RANS models due to the model constants using statistical methods such as Emory, Larsson & Iaccarino (2013), Edeling *et al.* (2014), Poroseva, Colmenares F. & Murman (2016) and Wang, Sun & Xiao (2016). The major takeaway from these studies is that the uncertainty in RANS model constants can be very high. Our finding demonstrates that the uncertainty is as high as 50 %.

Improvements in model constants have been attempted as multi-parameter optimization problems without considering the physics of the flow. Poroseva *et al.* (2016) highlighted the uncertainties in the model using DNS data for low-Reynolds-number zero pressure gradient flows to suggest an improved RANS-DNS framework. Xiong *et al.* (2022) recommended optimizing the closure coefficients to improve the accuracy using statistical methods. Ling, Kurzawski & Templeton (2016), Pan & Duraisamy (2018), Sotgiu *et al.* (2019), Li *et al.* (2022), Yan, Zhang & Chen (2022), Bounds, Uddin & Desai (2023) and Heo *et al.* (2024) have leveraged neural networks and machine learning to train models using the DNS data. Wang, Wu & Xiao (2017) attempted physics-informed machine learning of the LES/DNS data to obtain better coefficients.

Barring Eisfeld (2022), who discussed the importance of the equilibrium region in turbulence modelling at high Reynolds numbers, the context of equilibrium, or broadly flow physics, has escaped the eyes of other researchers. While evaluating the performance of machine learning algorithms, even Ling & Templeton (2015) have highlighted that the machine algorithms are opaque and physical insights are necessary.

Even though uncertainty in model constants has been studied extensively, to our knowledge, no recommendation has been made to update model constants that align RANS models with the state-of-the-art understanding of flow physics to improve their performance. The outcomes of statistical and machine learning studies have, at best, demonstrated the need to tighten the uncertainty. In the absence of consensus on the new value, the standard textbooks on turbulent flows (such as Pope 2000; Durbin & Reif 2011) have continued to recommend $C_\mu = 0.09$. However, considering the strong evidence, C_μ must be updated to a more physically appropriate value. Thus, we adopt a novel, yet simple, methodology to evaluate C_μ as discussed in the following section.

2. Towards a new value of C_μ

The equilibrium assumption ($\mathcal{P} \approx \epsilon$) holds well within the limit of 10 % beyond $y^+ = 30$, which marks the well-accepted onset of the logarithmic layer. Even though c^2 is not a constant, the average value of c^2 over the equilibrium region can provide a good estimate for C_μ .

We define a function g such that

$$g = \begin{cases} c^2, & 0.9 \leq \mathcal{P}/\epsilon \leq 1.1, \\ 0, & \text{otherwise.} \end{cases} \quad (2.1)$$

Then,

$$\overline{c^2} = \bar{g}. \quad (2.2)$$

Here, \bar{g} is the average of g in the range shown in figure 2. Thus, using the value of c^2 obtained from (2.2) in (1.5), the required value of C_μ for different Re_τ is obtained as shown in figure 4.

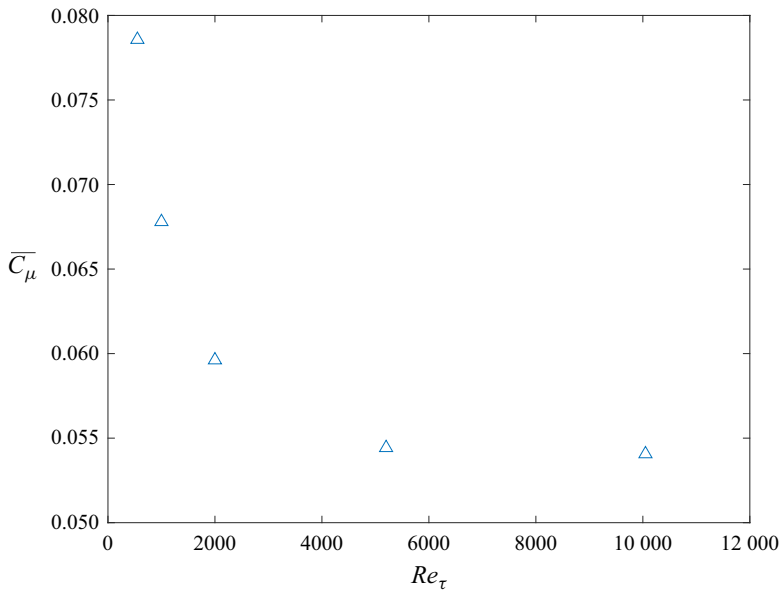


Figure 4. Plot of C_μ obtained using the value of c^2 averaged over the equilibrium region, as shown in figure 2.

3. Results and discussion

Figure 4 suggests that \overline{C}_μ approaches 0.06 at $Re_\tau = 5000$ and remains unchanged thereafter. Therefore, at sufficiently high Re_τ , \overline{C}_μ should become a constant, i.e. $C_\mu = 0.06$, against the parametrization suggested by Launder & Sharma (1974) in terms of turbulent Reynolds number $Re_T = k^2/\nu\epsilon$. For low Reynolds numbers, c^2 corroborates the prevalent value of 0.3.

Townsend (1976) reported the average stress–intensity ratio $c^2 = 0.26$ for all canonical flows. The corresponding C_μ as per Townsend’s (1976) $c^2 = 0.26$ would be 0.067, which is in close agreement with the trend shown in figure 4.

The impact of choosing $C_\mu = 0.06$ on predicting ν_T is shown in figure 5. For $Re_\tau = 10000$, $C_\mu = 0.06$ provides a closer agreement with the exact (DNS). Even though the near-wall prediction is still compromised due to high S (Karimpour & Venayagamoorthy 2013, 2014), it is much better in comparison to the classical value of $C_\mu = 0.09$. Also, the new value aligns with the physics of the turbulent flows, as revealed by recent DNS. In the atmospheric science community, c^2 is recommended as 0.17 for low-Richardson-number flows (Mauritsen *et al.* 2007; Wilson & Venayagamoorthy 2015). However, because of the inevitable shear layer in the outer region of the flow, it is questionable whether a robust recommendation can be made using the atmospheric boundary layer data. Recently, Eisfeld (2022), in his analysis, used the experimental values of Bradshaw *et al.* (1967) for the turbulent boundary layer and of Delville, Chahine & Bonnet (1987) for the plane mixing layer. While the turbulent boundary layer problem was at a very low Reynolds number, the values for the plane mixing layer have high uncertainties, leading to higher values of c^2 . Against Shih *et al.*’s (1994) proposal of parametrizing C_μ and introducing additional constants, the reduction in C_μ can be captured by changing the constant from 0.09 to 0.06.

Physically, a higher C_μ amplifies the turbulent viscosity based on the calculated values of k and ϵ . In a coarse grid, k and ϵ are poorly resolved, and the amplification of ν_T does not hamper the stability of the numerical code. However, in a finer mesh, k and ϵ are better resolved, and a higher C_μ destabilizes the code. Grid refinement in RANS models is primarily aimed at numerical accuracy. Ideally, a robust solution should be achievable on infinitely finer meshes, provided the other necessary numerical conditions (such as the Courant condition) are satisfied. However, obtaining grid independence in RANS

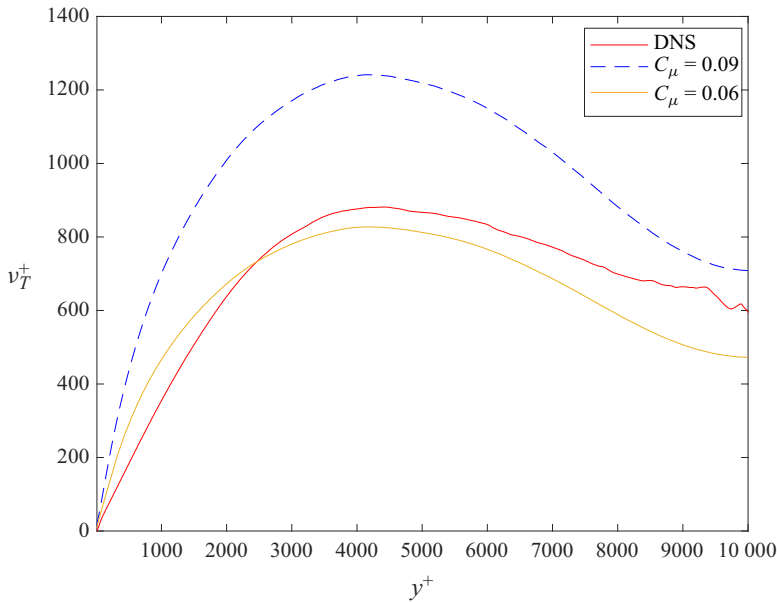


Figure 5. A priori comparisons of v_T with different values of C_μ using DNS data for $Re_\tau = 10\,000$ (Hoyas et al. 2022).

models is challenging (Celik 2003; Diskin et al. 2015). Improving closure constants could be a way to allow easier convergence with finer meshes.

A higher C_μ can also deteriorate the accuracy of the solution. For example, in a pollutant transport model, the model will show an early disappearance of the pollutant while it is still being transported (Mazarakis et al. 2016) due to artificial diffusion caused by higher v_T . This discrepancy has so far been handled through the calibration of models. Even though re-tuning of other closure constants (such as $C_{\epsilon 1}$, $C_{\epsilon 2}$, σ_ϵ) will be required to ensure complete accuracy, updating the turbulent viscosity parameter C_μ should be prioritized to ensure alignment of the $k-\epsilon$ model to the flow physics.

The existence of an asymptotic limit of c^2 , as shown in figure 4, can be explained using boundedness of turbulent quantities (Busse 1970). Since $c^2 = |\overline{uw}|/k$, $\overline{uw} \approx U_\tau^2(1 - z/h)$, where U_τ , z and h are the friction velocity, distance from the wall and the depth, respectively, we can deduce the stress-intensity ratio, $c^2 \approx (1 - z/h)/\overline{k^+}$. Recently, using the DNS data, Chen & Sreenivasan (2022) proposed a ‘final state’ of turbulence against the existing theory of endless variation. They argued that all wall quantities are bounded in the limit of an infinite Re_τ . Klewicki (2022) has supported this idea, but has pushed for stringent DNS at higher Re_τ to confirm this theory. The bounds suggest an asymptotic limit of k^+ . By similar reasoning, if $\lim_{Re_\tau \rightarrow \infty} \overline{k^+} = A(z/h)$, $\lim_{Re_\tau \rightarrow \infty} c^2 = (1 - z/h)/A(z/h)$, where A is the asymptotic function of $\overline{k^+}$ over z . If all bounded quantities asymptote, then the equilibrium region \mathbb{R} should also be identical. Thus, $\overline{c^2} = \overline{(1 - z/h)/A(z/h)}|_{\mathbb{R}} = B$, where B is the asymptotic limit of c^2 in the equilibrium region. We do not yet know A and B , but the data suggest that such an asymptotic function is plausible. We find Chen & Sreenivasan’s (2022) theory intuitive and it aligns with the trends shown by state-of-the-art DNS and experiments.

4. Limitations and future work

The standard $k-\epsilon$ model’s performance deteriorates in detached boundary layers, adverse pressure gradients and free-shear flows (Eisfeldt 2021). The values of C_μ could vary widely in free-shear flows, as reported by Lefantzi et al. (2014). Thus, even though the methodology has wider applications, the

findings of this paper are strictly applicable only to the attached wall-bounded turbulent flows. More experimental and DNS data are required to obtain a universal value of C_μ . Further, it is cautioned that merely changing C_μ to 0.06 might lead to inferior results because the other constants in the k - ϵ model have been tuned by fixing $C_\mu = 0.09$. Therefore, a wider comprehensive effort is required to re-tune the coefficients by setting C_μ to 0.06. This paper emphasizes that the parameter C_μ needs to be corrected first based on the latest DNS data. The fine-tuning of the model can be performed later once an agreement is achieved on the value of C_μ .

5. Conclusion

Using the data from DNS of highly turbulent channel flows, we have demonstrated that the current specification of turbulent viscosity parameter $C_\mu = 0.09$ in the k - ϵ model over-predicts the turbulent viscosity ν_T . We revisit the original specification of C_μ based on stress-intensity ratio $c^2 = |\overline{uw}|/k$ in the equilibrium region and find that even the maximum values of c^2 at high Reynolds number do not support the existing proposition of $C_\mu = 0.09$. We calculate a more appropriate value of $C_\mu = 0.06$ by averaging the stress-intensity ratio c^2 in the equilibrium region with a tolerance of 10%. A test using the new value of C_μ shows closer agreement with the exact values of ν_T obtained from the DNS in channel flows. Analysis has been presented to support the proposed modification to the k - ϵ model using the latest findings in the literature on turbulence theory. The trend suggests an asymptotic value of C_μ closer to 0.06.

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Author contributions. The initial idea was proposed by S.K.V. and H.M. prepared the manuscript.

Data availability statement. The DNS datasets used during the study were provided by a third party. Direct requests for DNS datasets may be made to the provider as indicated in the Acknowledgments.

Ethical standards. The research meets all ethical guidelines, including adherence to the legal requirements of the study country.

References

- BOIKOS, C., SIAMIDIS, P., OPPO, S., ARMENGAUD, A., TSEGAS, G., MELLQVIST, J., CONDE, V. & NTZIACHRISTOS, L. 2024 Validating CFD modelling of ship plume dispersion in an urban environment with pollutant concentration measurements. *Atmos. Environ.* **319**, 120261.
- BOUNDS, C.P., UDDIN, M. & DESAI, S. 2023 Tuning of turbulence model closure coefficients using an explainability based machine learning algorithm. *SAE Tech. Paper* 2023-01-0562. SAE International, Warrendale, PA.
- BRADSHAW, P., FERRISS, D.H. & ATWELL, N.P. 1967 Calculation of boundary-layer development using the turbulent energy equation. *J. Fluid Mech.* **28** (3), 593–616.
- BUSH, R.H., CHYCZEWSKI, T.S., DURAISAMY, K., EISFELD, B., RUMSEY, C.L. & SMITH, B.R. 2019 Recommendations for future efforts in RANS modeling and simulation. *AIAA Scitech 2019 Forum* 0317.
- BUSSE, F.H. 1970 Bounds for turbulent shear flow. *J. Fluid Mech.* **41** (1), 219–240.
- CELIK, I. 2003 RANS/LES/DES/DNS: the future prospects of turbulence modeling. *Trans. ASME J. Fluids Engng* **127** (5), 829–830.
- CHAMPAGNE, F.H., HARRIS, V.G. & CORRSIN, S. 1970 Experiments on nearly homogeneous turbulent shear flow. *J. Fluid Mech.* **41** (1), 81–139.
- CHEN, X. & SREENIVASAN, K.R. 2022 Law of bounded dissipation and its consequences in turbulent wall flows. *J. Fluid Mech.* **933**, A20.
- COTTON, M.A., GRAHAM, L., ISMAEL, J. & LAUNDER, B. 1992 First steps in the use of strain and vorticity invariants in two-equation modelling. In *Proceedings of the 5th Biennial CFD Colloquium UMIST*, vol. 1, p. 5.

- COTTON, M.A. & ISMAEL, J.O. 1998 A strain parameter turbulence model and its application to homogeneous and thin shear flows. *Intl J. Heat Fluid Flow* **19** (4), 326–337.
- DELVILLE, J., CHAHINE, Z. & BONNET, J.P. 1987 Experimental study of an incompressible, plane mixing layer by temporal and spectral analysis. In *Advances in Turbulence* (ed. G. Comte-Bellot & J. Mathieu), pp. 435–444. Springer.
- DISKIN, B., THOMAS, J.L., RUMSEY, C.L. & SCHWOPPE, A. 2015 Grid convergence for turbulent flows (Invited). In *53rd AIAA Aerospace Sciences Meeting*. American Institute of Aeronautics and Astronautics.
- DURASAMY, K., IACCARINO, G. & XIAO, H. 2019 Turbulence modeling in the age of data. *Annu. Rev. Fluid Mech.* **51** (1), 357–377.
- DURBIN, P.A. 2018 Some recent developments in turbulence closure modeling. *Annu. Rev. Fluid Mech.* **50**, 77–103.
- DURBIN, P.A. & REIF, B.A.P. 2011 *Statistical Theory and Modeling for Turbulent Flows*, 2nd edn. Wiley.
- DURBIN, P.A. & SHIH, T.-P. 2005 An overview of turbulence modeling. In *WIT Transactions on State of the Art in Science and Engineering*, 1st edn (ed. B. Sunden & M. Faghri), vol. 1, pp. 1–29. WIT Press.
- EDELING, W.N., CINNELLA, P., DWIGHT, R.P. & BIJL, H. 2014 Bayesian estimates of parameter variability in the k - ϵ turbulence model. *J. Comput. Phys.* **258**, 73–94.
- EISFELD, B. 2021 Characteristics of incompressible free shear flows and implications for turbulence modeling. *AIAA J.* **59** (1), 180–195.
- EISFELD, B. 2022 The importance of turbulent equilibrium for Reynolds-stress modeling. *Phys. Fluids* **34** (2), 025123.
- EMORY, M., LARSSON, J. & IACCARINO, G. 2013 Modeling of structural uncertainties in Reynolds-averaged Navier–Stokes closures. *Phys. Fluids* **25** (11), 110822.
- HANJALIC, K. 2005 Will RANS survive LES? A view of perspectives. *Trans. ASME J. Fluids Engng* **127** (5), 831–839.
- HARLOW, F.H. & NAKAYAMA, P.I. 1968 Transport of turbulence energy decay rate. *Tech. Rep.* Los Alamos National Laboratory (LANL), Los Alamos, NM.
- HARRIS, V.G., GRAHAM, J. A. H. & CORRSIN, S. 1977 Further experiments in nearly homogeneous turbulent shear flow. *J. Fluid Mech.* **81** (4), 657–687.
- HEO, S., YUN, Y., JEONG, M. & JEE, S. 2024 Simulation of supersonic axisymmetric base flow with a data-driven turbulence model. *Aerosp. Sci. Technol.* **147**, 109014.
- HOYAS, S., OBERLACK, M., ALCÁNTARA-ÁVILA, F., KRAHEBERGER, S.V. & LAUX, J. 2022 Wall turbulence at high friction Reynolds numbers. *Phys. Rev. Fluids* **7** (1), 014602.
- JONES, W.P. & LAUNDER, B.E. 1972 The prediction of laminarization with a two-equation model of turbulence. *Intl J. Heat Mass Transfer* **15** (2), 301–314.
- JONES, W.P. & LAUNDER, B.E. 1973 The calculation of low-Reynolds-number phenomena with a two-equation model of turbulence. *Intl J. Heat Mass Transfer* **16** (6), 1119–1130.
- KARIMPOUR, F. & VENAYAGAMOORTHY, S.K. 2013 Some insights for the prediction of near-wall turbulence. *J. Fluid Mech.* **723**, 126–139.
- KARIMPOUR, F. & VENAYAGAMOORTHY, S.K. 2014 A revisit of the equilibrium assumption for predicting near-wall turbulence. *J. Fluid Mech.* **760**, 304–312.
- KLEWICKI, J.C. 2022 Bounded dissipation predicts finite asymptotic state of near-wall turbulence. *J. Fluid Mech.* **940**, F1.
- KOLMOGOROV, A.N. 1941 Equations of turbulent motion in an incompressible fluid. *Dokl. Akad. Nauk* **30**, 299–303.
- LAUNDER, B.E., MORSE, A., RODI, W. & SPALDING, D. 1973 Prediction of free shear flows: a comparison of the performance of six turbulence models. In *Free Turbulent Shear Flows*, vol. 1. NASA Langley Research Center.
- LAUNDER, B.E. & SHARMA, B.I. 1974 Application of the energy-dissipation model of turbulence to the calculation of flow near a spinning disc. *Lett. Heat Mass Transfer* **1** (2), 131–137.
- LAUNDER, B.E. & SPALDING, D. 1974 The numerical computation of turbulent flows. *Comput. Meth. Appl. Mech. Engng* **3** (2), 269–289.
- LEFANTZI, S., RAY, J., ARUNAJATESAN, S. & DECHANT, L. 2014 Estimation of k - ϵ parameters using surrogate models and jet-in-crossflow data. *Tech. Rep.* SAND2015-0707. Sandia National Laboratory (SNL-CA), Livermore, CA; Sandia National Laboratory (SNL-NM), Albuquerque, NM.
- LI, J.-P., TANG, D.-G., YI, C. & YAN, C. 2022 Data-augmented turbulence modeling by reconstructing Reynolds stress discrepancies for adverse-pressure-gradient flows. *Phys. Fluids* **34** (4), 045110.
- LING, J., KURZAWSKI, A. & TEMPLETON, J. 2016 Reynolds averaged turbulence modelling using deep neural networks with embedded invariance. *J. Fluid Mech.* **807**, 155–166.
- LING, J. & TEMPLETON, J. 2015 Evaluation of machine learning algorithms for prediction of regions of high Reynolds averaged Navier Stokes uncertainty. *Phys. Fluids* **27** (8), 085103.
- MAURITSEN, T., SVENSSON, G., ZILITINKEVICH, S.S., ESAU, I., ENGER, L. & GRISOGONO, B. 2007 A total turbulent energy closure model for neutrally and stably stratified atmospheric boundary layers. *J. Atmos. Sci.* **64** (11), 4113–4126.
- MAZARAKIS, N., KALOUDIS, E., NAZOS, A. & NIKAS, K.-S.P. 2016 Les and rans comparison of flow and pollutant dispersion in urban environment. *Intl J. Environ. Stud.* **73** (1), 48–65.
- PAN, S. & DURASAMY, K. 2018 Data-driven discovery of closure models. *SIAM J. Appl. Dyn. Syst.* **17** (4), 2381–2413.
- POPE, S.B. 2000 *Turbulent Flows*. Cambridge University Press.
- POROSEVA, S.V., COLMENARES F., J.D. & MURMAN, S.M. 2016 On the accuracy of RANS simulations with DNS data. *Phys. Fluids* **28** (11), 115102.

- PRANDTL, L. 1945 Ueber ein neues formelsystem für die ausgebildete turbulenz. In *Nachrichten der Akademie der Wissenschaften in Göttingen. Mathematisch-Physikalische Klasse*, pp. 6–18.
- REYNOLDS, W. 1987 Fundamentals of turbulence for turbulence modeling and simulation. In *Lecture Notes for Von Karman Institute Agard Report*, vol. 755, 005793. Von Karman Institute.
- RODI, W. 1972 The prediction of free turbulent boundary layers by use of a two-equation model of turbulence. PhD thesis, University of London.
- RODI, W. 2017 Turbulence modeling and simulation in hydraulics: a historical review. *J. Hydraul. Engng* **143** (5), 03117001.
- SHIH, T.-H., LIOU, W.W., SHABBAR, A., YANG, Z. & ZHU, J. 1994 A new $k-\epsilon$ eddy viscosity model for high Reynolds number turbulent flows: model development and validation. *Tech. Rep. CMOTT-94-6*. NTRS Document ID: 19950005029. Legacy CDMS (CDMS). NASA Lewis Research Center.
- SHIH, T.-H., LIOU, W.W., SHABBAR, A., YANG, Z. & ZHU, J. 1995 A new $k-\epsilon$ eddy viscosity model for high Reynolds number turbulent flows. *Comput. Fluids* **24** (3), 227–238.
- SINCLAIR, J.M., VENAYAGAMOORTHY, S.K. & GATES, T.K. 2022 Some insights on flow over sharp-crested weirs using computational fluid dynamics: implications for enhanced flow measurement. *J. Irrig. Drain. Engng* **148** (6), 04022011.
- SOTGIU, C., WEIGAND, B., SEMMLER, K. & WELLINGER, P. 2019 Towards a general data-driven explicit algebraic Reynolds stress prediction framework. *Intl J. Heat Fluid Flow* **79**, 108454.
- SUGA, K. 1995 Development and application of a non-linear eddy-viscosity model sensitized to stress and strain invariants. PhD, The University of Manchester (UK).
- TAVOULARIS, S. & CORRSIN, S. 1981 Experiments in nearly homogenous turbulent shear flow with a uniform mean temperature gradient. Part 1. *J. Fluid Mech.* **104**, 311–347.
- TOWNSEND, A. 1976 *The Structure of Turbulent Shear Flow*. Cambridge University Press.
- VASSILICOS, J.C. 2015 Dissipation in turbulent flows. *Annu. Rev. Fluid Mech.* **47** (1), 95–114.
- WANG, J.-X., SUN, R. & XIAO, H. 2016 Quantification of uncertainties in turbulence modeling: a comparison of physics-based and random matrix theoretic approaches. *Intl J. Heat Fluid Flow* **62**, 577–592.
- WANG, J.-X., WU, J.-L. & XIAO, H. 2017 Physics-informed machine learning approach for reconstructing Reynolds stress modeling discrepancies based on DNS data. *Phys. Rev. Fluids* **2** (3), 034603.
- WILSON, J.M. & VENAYAGAMOORTHY, S.K. 2015 A shear-based parameterization of turbulent mixing in the stable atmospheric boundary layer. *J. Atmos. Sci.* **72** (5), 1713–1726.
- XIONG, M., CHEN, B., ZHANG, H. & QIAN, Y. 2022 Study on accuracy of CFD simulations of wind environment around high-rise buildings: a comparative study of $k-\epsilon$ turbulence models based on polyhedral meshes and wind tunnel experiments. *Appl. Sci.* **12** (14), 7105.
- XU, J., SUN, G. & XU, D. 2020 Distribution of stress intensity ratio in canonical turbulent flows and converging-diverging channel. *Acta Astronaut.* **166**, 342–349.
- YAKHOT, V. & ORSZAG, S.A. 1986 Renormalization group analysis of turbulence. I. Basic theory. *J. Sci. Comput.* **1** (1), 3–51.
- YAN, C., ZHANG, Y. & CHEN, H. 2022 Data augmented turbulence modeling for three-dimensional separation flows. *Phys. Fluids* **34** (7), 075101.